Design of Neural Network Predictive Controller for a Quadruple Tank System

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Abstract-- The processes in most of the industries are highly non-linear and dynamic. The quadruple tank system is a benchmark system used to analyse the nonlinear effects in a multivariable process. The quadruple tank process is thus used to demonstrate coupling effects and interactions occurring in multivariable control systems. This project presents a neural network predictive controller for a quadruple tank system. The process data will be obtained from the mathematical model of the laboratory scale experimental setup. The model obtained from training the system via neural network will be used in controlling the quadruple tank by neural network predictive controller. The simulation results will be compared with the closed loop response and constrained and unconstrained model predictive control algorithm results.

Index Terms- Quadruple tank system, MPC, Neural Network

I. INTRODUCTION

Most of industrial control problems are non linear and have multiple controlled variables which in turn leads to significant uncertainties, strong interactions, and non-minimum phase behavior.[12] So it is important for control system engineers to understand the problems of industrial processes by carrying out experiments with a good laboratory apparatus. The quadruple tank setup is a well known process used as a standard experiment for students and for control related research activities. The primary application of the quadruple tank process is to study and test MIMO control, as it provides a simple non linear 2x2 system with interactions and non- minimum phase behaviours.

Model predictive control techniques are widely used in the process industries and are considered as methods that give good performance without almost any intervention. However the main reason that model predictive control is popular in industry is that it is the only technique that allows system restrictions to be taken into consideration. Most of the industrial processes have non linear dynamics. But most MPC applications are based on linear models. However there are processes that can't be represented by a linear model and require the use of non linear models. This gives rise to the use of non linear model predictive controller. In this project Neural Network based non linear model predictive controller is implemented for a quadruple tank system. The block diagram is shown in Figure 1.



Fig. 1 Block diagram of neural network predictive controller for quadruple tank system

II. PROCESS DESCRIPTION

The quadruple tank is a laboratory process with four tanks that are interconnected, and two pumps as shown in Figure 3. The process inputs are input flow rates of the two pumps, 0-1000 lph and the outputs are levels of lower two tanks, 0-250mm. Our aim is to control the levels of the lower two tanks. The practical quadruple tank setup is shown in Figure 2. The outputs of the two pumps are split into two using a three-way valve. Pump 1 is shared by tank 1 and tank 3 and pump 2 is shared by tank 2 and tank 4. Thus each pump output goes to two tanks, one lower and another upper diagonal tank and the flow to these tanks are controlled by the position of the valve represented as γ . The position of the valves determines whether the system will

operate in the minimum phase or in the nonminimum phase. [5]

All the tanks have a discharge valve at the bottom. The discharge from tank 4 goes to tank 1 while discharge of tank 3 goes to tank 2. This interaction is a major problem in a multivariable control system. Discharge from tank1 and tank 2 goes to the reservoir tank at the bottom. [5]



Fig. 2 Quadruple tank system setup



Fig. 3 Schematic diagram of a quadruple tank system

III. NEURAL NETWORK PREDICTIVE CONTROLLER

The neural network predictive controller uses a neural network model of a plant to predict future plant performance. The controller then optimizes plant performance over a specified time horizon by calculating control input. The first step is to determine the neural network plant model. Then, the plant model is used by the controller to predict future performance. The block diagram of neural network predictive controller is shown in Figure 4.

A. System Identification

The first stage of model predictive control is to train a neural network to represent the forward dynamics of the plant. Neural network training signal is the prediction error between the plant output and the neural network output. The process is represented by the Figure 5. The neural network plant model uses previous inputs and plant outputs to predict future values of the plant output. The neural network plant model structure is given in the following Figure 6.



Fig. 4 Neural network predictive controller



Fig. 5 Neural network training

B. Predictive Control

Model predictive control is based on the receding horizon technique. The neural network model predicts the response of the plant over a specified time horizon. The predictions are used by a numerical optimization program to determine the control signal that minimizes the performance criterion over the specified horizon. [1]



Fig. 6 Structure of neural network plant model

IV. RESULTS AND DISCUSSION

A. Simulation of PI Controller

The PI controller response of quadruple tank process for a minimum phase system is obtained as shown in Figure 7. The settling time is 150 sec for both tanks while the rise time for tank 1 is 9 sec and that of tank 2 is 2 sec. Peak Overshoot of tank 1 is 44% and that of tank 2 is 140%. ISE obtained are 1794 and 2094 for tanks 1 and 2 respectively. The PI controller response of quadruple tank process for non minimum phase system is shown in Figure 8. The settling time is 220 sec for both tanks while the rise time for tank 1 is 20 sec and that of tank 2 is 10 sec. Peak Overshoot of tank 1 is 9.33% and that of tank 2 is 100%. ISE obtained are 2327 and 2831 for tanks 1 and 2 respectively.

B. Simulation of Constrained MPC

Constrained MPC is an MPC in which the constraints of the system are specified. The constrained MPC response of the quadruple tank process for minimum phase system is given in Figure 9. The settling time is 110 sec for both tanks while the rise time for tank 1 is 32 sec and that of tank 2 is 27 sec. Peak Overshoot of tank 1 is 8.6% and that of tank 2 is 6%. ISE obtained are 745 and 242 for tanks 1 and 2 respectively. The constrained MPC response of the quadruple tank process for non minimum phase system is given in Figure 10. The settling time is 150 sec for both tanks while the rise time for tank 1 is 38 sec and that of tank 2 is 34 sec. ISE obtained are 727 and 3382 for tanks 1 and 2 respectively.

C. Simulation of Unconstrained MPC

Unconstrained MPC is an MPC in which the constraints of the system are not specified. The unconstrained MPC response of the quadruple tank

process for minimum phase system is given in Figure 11. The settling time is 56 sec for both tanks while the rise time for tank 1 is 25 sec and that of tank 2 is also 25 sec. Peak Overshoot of tank 1 is 2.6% and that of tank 2 is 2.5%. ISE obtained are 396 and 188 for tanks 1 and 2 respectively. The unconstrained MPC response of the quadruple tank process for non minimum phase system is given in Figure 12. The settling time is 150 sec for both tanks while the rise time for tank 1 is 20 sec and that of tank 2 is 24 sec. Peak Overshoot of tank 2 is 10%. ISE obtained are 886 and 3111 for tanks 1 and 2 respectively.

D. Simulation of Neural Network Predictive Controller

The response of a neural network predictive controller for quadruple tank process with minimum phase is given in Figure 13. The settling time is 45 sec for both tanks while the rise time for tank 1 is 2.8 sec and that of tank 2 is 2.3 sec. Peak Overshoot of tank 1 is 58% and that of tank 2 is 50%. ISE obtained are 484 and 247 for tanks 1 and 2 respectively. The response of a neural network predictive controller for quadruple tank process with non minimum phase is given in Figure 14. The settling time is 100 sec for both tanks while the rise time for tank 1 is 1.6 sec and that of tank 2 is 1.5 sec. Peak Overshoot of tank 1 is 182% and that of tank 2 is 189%. ISE obtained are 844 and 634 for tanks 1 and 2 respectively.

E. Performance Analysis

The performance of the controllers is validated by comparing the settling time, rise time, peak overshoot and Integral Square Error (ISE). The results for minimum phase and non minimum phase systems are tabulated below in Table 1. It is seen that neural network predictive controller show better performance over MPC and PI controllers.

V. CONCLUSION AND FUTURE SCOPE

Comparative study of the performance of PI controller, Constrained and Unconstrained MPC and Neural Network based Non linear Model Predictive Controller for a quadruple tank system has been done. Quadruple tank system is a classical MIMO non linear system cable of operating in both minimum and non minimum phase behaviors.

Performance comparison for both cases has been done.

It is seen that neural network based non linear model predictive controller is able to provide superior performance in case of settling time, rise time and Integral Square Error (ISE). Therefore this method can be adopted for the control of other non linear systems very efficiently compared to traditional control algorithms and linear MPC.



Response of PI Controller for a Non Minimum Phase Quadruple Tank System
System
Set point 1
Set point 1
Level 1



Fig. 8 Response of PI controller for non minimum phase system



g. 9 Response of constrained MPC for non minimu phase system



Fig. 10 Response of constrained MPC for minimum phase system







Fig. 12 Response of unconstrained MPC for non minimum phase system



for minimum phase system



Fig. 14 Response of neural network predictive controller for non minimum phase system

Minimum Phase								
Parameter	PI		Constrained MPC		Unconstrained MPC		NMPC	
	tank 1	tank 2	tank 1	tank 2	tank 1	tank 2	tank 1	tank 2
Settling Time (sec)	150	150	110	110	56	56	45	45
Rise time (sec)	9	2	32	27	25	25	2.8	2.3
Peak Overshoot (%)	44	140	8.6	6	2.6	2.5	58	50
ISE	1794	2094	745	242	396	188	284	147
Non Minimum Phase								
Parameter	PI		Constrained MPC		Unconstrained MPC		NMPC	
	tank 1	tank 2	tank 1	tank 2	tank 1	tank 2	tank 1	tank 2
Settling Time (sec)	220	220	150	150	150	150	100	100
Rise time (sec)	20	10	38	34	20	24	1.6	1.5
Peak Overshoot (%)	9.33	100	-	-	-	10	182	189
ISE	2327	2831	727	3382	886	3111	844	634

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